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(21) International Application Number: PCT/US00/06010 (22) International Filing Date: 08 March 2000 (08.03.2000) (30) Priority Data: 09/287,591 06 April 1999 (06.04.1999) US (60) Parent Application or Grant MASSACHUSETTS INSTITUTE OF TECHNOLOGY [/]; O. GEIS, Michael, W. [/]; O. KUNZ, Roderick, R. [/]; O. STERN, Margaret, B. [/]; O. SHAPIRO, Heather, B. ; O.		Published
(54) Title: THERMOPHORETIC PUMP AND CONCENTRATOR (54) Titre: POMPE ET CONCENTRATEUR THERMOPHORETIQUES (57) Abstract <p>The method and apparatus of the invention create a dynamic Soret effect for propelling a target chemical constituent along a pathway. A moving temperature profile impressed upon the pathway produces consecutive alternating warmer and cooler zones along the path which transport components of a mixture down the path according to their respective diffusivities. In one embodiment, the invention provides a dynamic thermophoretic concentrator for separating a target chemical constituent from a mixture of components on the basis of diffusion coefficient by using alternate forward and backward motion of a temperature profile along the pathway, thereby accumulating an ultimate concentration of the target constituent greater than its initial concentration in the mixture.</p> (57) Abrégé <p>Le procédé et l'appareil selon l'invention permettent de créer un effet Soret dynamique destiné à propulser un constituant chimique cible le long d'une voie d'écoulement. Un profil de températures variable appliqué à ladite voie permet de produire une alternance de zones chaudes et froides consécutives le long de la voie transportant les composants d'un mélange vers le bas selon leurs coefficients de diffusion respectifs. Selon un mode de réalisation, l'invention concerne un concentrateur thermophorétique dynamique permettant de séparer un constituant chimique cible d'un mélange de composants sur la base de leur coefficient de diffusion, et ce par utilisation des mouvements avant-arrière alternés d'un profil de températures le long de la voie, ce qui permet d'accumuler une concentration finale du constituant cible supérieure à sa concentration initiale dans le mélange.</p>		

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Description

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THERMOPHORETIC PUMP AND CONCENTRATOR

This invention was made with government support under contract number F19628-95-C-0002 awarded by the Air Force. The government has certain rights in this invention.

BACKGROUND OF THE INVENTION

Detection of trace amounts of illicit substances such as explosives and narcotics is an ever more critical element of combating terrorism and contraband. However, the exacting operating requirements a detector must meet in order to be useful for these purposes severely limit the number of suitable technologies.

The primary operating requirement is sensitivity. Many of the materials targeted by law enforcement or security screenings are present in the gas phase at very low fractional molecular concentrations. Table 1 shows approximate values of room-temperature vapor pressures for common explosives and cocaine, reports of which often vary by as much as an order of magnitude.

Table 1

<u>explosive</u>	<u>vapor pressure in air at room temperature (atm)</u>
glycerol trinitrate ("NG")	10^{-7}
2,4,6 trinitrotoluene ("TNT")	10^{-8}
1,3,5-trinitro-1,3,5-triazacyclohexane ("RDX")	10^{-12}
pentaerythritol tetranitrate ("PETN")	4×10^{-13}
C-4 (due to plasticizer and RDX)	10^{-14}
cocaine	10^{-10}

5 Realistic use in demanding security environments, entailing screening thousands
of containers per day, would further require that each determination be completed
10 rapidly, in well under a second. For many law enforcement situations, a serviceable
illicit substance detector would necessarily be portable.

15 Many sensing devices have been proposed for detecting trace amounts of
explosives or drugs in security or law enforcement contexts. However, none has
combined the sensitivity to detect constituents present at concentrations as low as 10^{-12}
20 atm with the requisite rapidity and portability.

For example, a bioluminescence-based explosives detection and identification
10 system capable of detecting constituents in air having a fractional molecular
25 concentration on the order of 10^{-14} has been proposed. However, the required
processing time is on the order of several minutes. (See, e. g., E. M. Boncyk in *Proc.*
30 *3rd Int. Symp. on Analysis and Detection of Explosives*, Mannheim-Neuostheim,
Germany, 4.1-40.14 [1989].)

15 Ion mobility spectrometry ("IMS") has found wide application as a relatively
35 quick and accurate technology for detecting explosives and illicit drugs. The nominal
sensitivity of IMS-based systems ranges from about 10^{-12} to 10^{-14} atm. As is typical of
40 gas-phase sensors, the minimum level of a target compound detectable by this
technique is limited by false positives and interference from other gaseous constituents
20 rather than by the inherent capability of the sensor.

45 The reliance of standard IMS on the ion charge-to-mass ratio to differentiate
constituents predisposes it to false positives when used to detect explosives or drugs.
50 For example, the ion mobility spectrum obtained from methamphetamine, a product of

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5 cocaine decomposition, overlaps on the time axis with that due to a common skin
conditioner ingredient, so that this ingredient provokes a false positive by an ion
10 mobility spectrometer configured to detect methamphetamine. Introducing an ionizable
vapor dopant that neutralizes the problematic skin conditioner ingredient but not
15 molecules of explosives or methamphetamine—which have exceptionally large electron
or proton affinities—mitigates this difficulty, but at the expense of some increase in
system complexity. Impurities remaining in the sensor from a previous screening are
20 another significant source of error in IMS-based systems.

Also, substances such as RDX and PETN having vapor pressures near the lower
10 limits of detectability by IMS can be detected by this method only after several seconds
25 of sampling. Such an interval is unacceptably long for high-volume applications, such
as comprehensive passenger screening at airports.

BRIEF DESCRIPTION OF THE INVENTION

Objects of the invention

35 It is, accordingly, an object of the present invention to provide method and
apparatus for enhancing the capability of detectors with respect to trace constituents.

40 It is another object of the present invention to provide method and apparatus or
eliminating interfering background impurities prior to subsequent downstream
45 20 detection.

It is another object of the invention to provide method and apparatus for rapidly
50 detecting trace constituents.

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5 It is another object of the invention to reduce the occurrence of false positives in
ion mobility spectrometry systems.

10 It is another object of the invention to provide method and apparatus that allow
easy and quick clearing of a sensor system.

15 5 It is yet another object of the invention to provide suitable method and apparatus
for detecting illicit drugs and explosives and decomposition products thereof in law
enforcement and security environments.

Summary of the Invention

25 10 The invention provides method and apparatus for propelling a target chemical
constituent, or equivalently a set of constituents, along a pathway by applying a time-
varying temperature profile along the pathway so as to effect a dynamic Soret effect.
30 The temperature profile impressed upon the pathway creates at least one region over
which temperature varies with position, so as to produce a warmer zone and a cooler
35 15 zone situated consecutively along the path. In accordance with the Soret effect,
components present at dilute concentration in a carrier medium segregate in the
temperature gradient according to their respective molecular weights. Components
40 having molecular weights greater than that of the carrier medium accumulate in the
cooler zone, whereas components having higher molecular weights diffuse toward the
45 20 warmer zone. In moving to establish this thermally driven concentration gradient, each
component advances toward the appropriate portion of the temperature profile at a
respective net average velocity known to those of skill in the art as its Soret velocity.
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In accordance with the invention, the region of temperature variation is displaced along the pathway at a wave velocity, so as to generate a time-varying temperature profile. As the local temperature changes, the segregated dilute components move so as to preserve or reestablish the thermally induced concentration gradient. Thus the components are conveyed along the pathway with the moving region of temperature variation. The quantity of a particular constituent that is pumped down the path depends on the temperature gradient, the absolute value of the wave velocity and its relative value compared to the constituent's Soret velocity, and also the diffusion coefficient of the constituent in the carrier medium.

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In one embodiment, the invention provides a dynamic thermophoretic concentrator for separating a target chemical constituent from a mixture of components on the basis of diffusion coefficient by using alternate forward and backward motion of the temperature profile along the pathway, thereby accumulating an ultimate concentration of the target constituent greater than its initial concentration in the mixture by a factor up to ten, 100, 10^3 , 10^4 or even greater. Because most components have very similar Soret velocities, as a practical matter the distribution of a constituent across a given moving temperature profile depends mainly on its diffusion coefficient. Particles having small diffusion coefficients, correlating with large particle sizes, are concentrated in the cooler portion of the temperature profile more compactly, and thus transported at a greater flux by the time-varying profile; the degree of localization drops rather abruptly with increasing diffusion coefficient, so that smaller constituents are distributed more evenly throughout the region of varying temperature and less efficiently transported. The diffusion coefficient at which the flux declines can be

5 shifted to higher values by increasing the temperature difference between the warmer
and cooler extremes. For a given temperature gradient, the basic shape of the flux-
10 diffusivity function changes with the wave velocity.

In accordance with the invention, the temperature profiles and wave velocities
15 used for forward and backward motion are chosen in conjunction to enhance the net
forward flux of a target constituent, and suppress that of other constituents, based on
diffusivities, thereby preferentially conveying the target constituent forward. For
20 example, distinct forward and backward thermal profiles, differing from one another in
shape or temperature gradient, may be used. Or, in a preferred embodiment, a single
10 temperature profile is moved at different forward and backward wave velocities. In
particular, a target constituent is concentrated at an end of the pathway by alternately
moving the temperature profile toward the end at a forward wave velocity greater than
25 the constituent's Soret velocity and away from the end at a backward wave velocity less
than the constituent's Soret velocity.
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15 The invention is compatible with micrometer-scale implementation, allowing
35 for a reduction in both concentration time and power requirement compared to
concentrators known in the art. Its speed and portability suit it for security and law
40 enforcement applications and its sensitivity is equal to detecting residues of explosives
and narcotics or their decomposition products. To this end, the thermophoretic
20 concentrator of the invention is particularly advantageous when used in conjunction
45 with a fluid phase detector, for example an ion-mobility spectrometer. The use of
diffusivity as a discriminator enables ion-mass spectrographic systems to differentiate
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between a target constituent and other, confounding dilute components, thereby abating false positive indications.

The ability to selectively preconcentrate an arbitrary dilute constituent by several orders of magnitude and also to eliminate background impurities before subsequent downstream detection mitigates the limitation on minimum detectable constituent level inherent to most gas-phase sensors. Furthermore, by wholesale backward pumping the dynamic thermophoretic concentrator of the invention is able to clear the system of extraneous impurities between uses in less time than is required to detect a target constituent.

BRIEF DESCRIPTION OF THE DRAWINGS

The invention description below refers to the accompanying drawings, not necessarily to scale, of which:

FIG. 1 graphically depicts the concentration enhancement of dilute constituents in gaseous nitrogen between a cooler region at $T_{Low} = 100\text{ }^{\circ}\text{C}$ and a warmer region at $T_{High} = 300\text{ }^{\circ}\text{C}$;

FIG. 2 shows the approximate dependence of thermal diffusion velocity coefficient on constituent particle size in gaseous nitrogen;

FIGs. 3A through 3C schematically depicts constituent concentration in the cooler zone of a thermal profile including a region over which temperature is a nonconstant function of position, wherein FIG. 3A illustrates a stationary or relatively slowly-moving profile, and FIGs. 3B and 3C illustrate more rapidly moving profiles;

FIG. 4 shows a thermal profile having a series of alternating cooler and warmer zones along the pathway;

FIG. 5 graphically depicts the modeled normalized flux carried by moving thermal profiles as a function of constituent diffusivity;

FIG. 6 graphically depicts the net normalized flux carried by a bidirectionally moving thermal profile as a function of constituent diffusivity;

FIG. 7 graphically depicts the calculated concentration of constituents resulting from bidirectional pumping as a function of diffusivity;

FIG. 8 shows, in cross-section, an apparatus for pumping a chemical constituent along a pathway; and

FIG. 9 shows an annular member bearing two interspersed serpentine heating elements.

DETAILED DESCRIPTION OF AN ILLUSTRATIVE EMBODIMENT

When a thermal gradient is impressed on a gas mixture in a closed container, the components thermophoretically diffuse until an equilibrium concentration is reached.

The partial pressure ratio of a constituent i

$$R_i = \frac{X_{iLow}}{X_{iHigh}},$$

in which X_{iHigh} and X_{iLow} are the ratios of the constituent's partial pressure to the total pressure in the higher and lower temperature regions, respectively. R_i depends on the high and low temperatures in the container, T_{High} and T_{Low} , and the thermophoresis coefficient α_j for the constituent i in carrier medium j as follows:

$$R_i = \frac{X_{iLow}}{X_{iHigh}} = \left[\frac{T_{Low}}{T_{High}} \right]^{\alpha_i}.$$

For example, a temperature difference of a few hundred degrees centigrade in a carrier gas of nitrogen can cause higher molecular weight gases to increase their partial pressures by more than 100% in the lower temperature region. FIG. 1 shows the normalized absolute concentration increase for several dilute constituents in gaseous nitrogen between a cooler zone at $T_{Low} = 100$ °C and a warmer zone at $T_{High} = 300$ °C. The solid line 12 is calculated for constituents having molecular weights greater than 40 atomic mass units. (The thermophoretic data presented herein for TNT and RDX is estimated from their molecule sizes and from published data for both smaller and larger components in nitrogen.)

Molecules of each constituent i undergoing thermally driven diffusion move at a respective average thermal drift velocity

$$V_{i, Soret} = \Theta_i \frac{dT}{dx} = \frac{D_{ij} \alpha_{ij}}{T} \frac{dT}{dx},$$

in which Θ_i is the constituent's thermal diffusion velocity coefficient, D_{ij} is its diffusion coefficient in the carrier gas, T is the local temperature, and $\frac{dT}{dx}$ is the local thermal gradient. In FIG. 2, curve 22 approximately shows the dependence of thermal diffusion velocity coefficient on dilute constituent particle size in gaseous nitrogen. For particles having diameters from about 1 nanometer to about 1 micrometer in diameter, variations in diffusion and thermophoresis coefficients are roughly compensatory so that constituents in this range have nearly the same value of Θ_i , on the order of $2.4 \times$

5 $10^{-4} \text{ cm}^2 \text{ s}^{-1} \text{ K}^{-1}$. (For smaller constituents, the force generated by the thermal gradient
does not scale as neatly with size but rather depend on details of the intermolecular
10 interactions and approaches zero as the size and molecular weight of the dilute
constituent approach that of the carrier gas.) However, the magnitude of V_{Soret} for
15 species in this size range can be adjusted by choice of the thermal gradient.

FIG. 3A shows a thermal profile including a region over which temperature is a
nonconstant function of position so as to encompass a cooler zone 20 and a warmer
20 zone 22 along an axis defining a pathway. Molecules of a dilute constituent having a
greater molecular weight than that of the carrier gas collect preferentially in the cooler
10 zone 20, as represented by circles 24. If, in accordance with the invention, the region of
nonconstant temperature is displaced along the pathway at a thermal wave velocity
 V_{wave} , the local constituent distribution adjusts so as to maintain the thermally induced
30 concentration gradient as the local temperature changes. If the thermal wave velocity is
less than the Soret velocity, the thermally induced drift is sufficiently rapid to follow
15 the temperature profile motion, so that the aggregation of the constituent in the cooler
zone 20 is preserved as depicted in FIG. 3A. Under these conditions, the moving cooler
zone is able to efficiently transport dilute constituent. As V_{wave} increases, the degree of
40 constituent confinement in the cooler zone diminishes, as depicted in FIG. 3B, in which
the wave and Soret velocities are comparable, and FIG. 3C, for which the wave velocity
20 is greater than the Soret velocity. As V_{wave} surpasses V_{Soret} the constituent distribution
45 approaches uniformity along the pathway. Transport of dilute constituent by the cooler
zone 20 becomes less efficient.

Since most components have similar Soret velocities, for a given thermal wave velocity, the extent to which one dilute constituent is confined to the moving cooler zone, compared to another constituent, is largely determined by the relative values of the constituents' diffusivities. Large particles greater than 2 nanometers in diameter, generally having values of D_j less than $0.01 \text{ cm}^2 \text{ s}^{-1}$, have comparatively large values of α_{ij} , and are relatively easily concentrated in the cooler zone. The intermediate diffusivities of, for example RDX, TNT and cocaine, on the order of $0.04 \text{ cm}^2 \text{ s}^{-1}$, afford somewhat less concentration. Small particles, such as common air components oxygen, carbon dioxide, argon and xenon, have diffusivities greater than $0.1 \text{ cm}^2 \text{ s}^{-1}$ and tend to scatter more uniformly along the path.

FIG. 4 shows a symmetrical sawtooth temperature profile comprising a series of alternating cooler 20 and warmer 22 zones and along the pathway. For a dilute constituent having a given diffusivity, the effect that displacing such a series of zones along the path has on the constituent distribution along the pathway is determined by the temperature difference ΔT of the sawtooth profile and by the thermal wave velocity. In accordance with the invention, adjusting these operating parameters tailors the composition of the fluid selected from the component mixture and moved by the time-varying temperature profile, on the basis of constituents' diffusivities.

With reference to FIG. 5, the modeled normalized flux as a function of constituent diffusivity is illustrated by curve 40 for a sawtooth profile with $\Delta T = 50^\circ \text{C}$ moving at $V_{\text{wave}} = 0.1 V_{\text{Soret}}$, assuming that the components of the fluid mixture do not adhere to the surfaces defining the pathway. The flux declines as D_j exceeds about $5 \times 10^{-4} \text{ cm}^2 \text{ s}^{-1}$. In comparison, the knee of curve 42, corresponding to $\Delta T = 200^\circ \text{C}$, is

5 shifted to higher diffusivity values. The declivity of curve 44, for which $\Delta T = 200^\circ\text{C}$
and $V_{\text{wave}} = 3 V_{\text{Soret}}$, is more shallow, so that the relative flux of the higher-diffusivity
10 constituents, compared to that of the lower-diffusivity components, is enhanced. In this
case, the smaller quantity of constituent carried in each cooler zone 20 at high wave
15 velocities is offset by the much greater number of zones traversing the path per unit
time; even constituents very poorly contained in a zone are transported in some
quantity. (Please note that for illustration purposes, the low-diffusivity plateaus of the
20 flux curves 40, 42 and 44 are all normalized to a common value. In fact, as diffusivity
approaches zero, so that perfect confinement is achieved, the faster-moving profile must
10 produce a greater flux than does the slower one.)

In a preferred embodiment, the invention incorporates displacement of the
region of nonconstant temperature alternately in opposite directions, thereby
30 concentrating a target constituent. FIG. 6 demonstrates the use of such bidirectional
thermophoretic pumping to concentrate from a dilute gaseous solution only those
15 constituents belonging to a selected portion of the diffusivity spectrum. Corresponding
to a profile with $\Delta T = 200^\circ\text{C}$ and $V_{\text{wave}} = 3 V_{\text{Soret}}$ as depicted by curve 42, curve 62
represents the diffusivity profile of the fluid components transported by a forward-
40 moving sawtooth. Curve 64 corresponds to curve 44 and represents the same pattern
and gradient moving backward at $V_{\text{wave}} = 0.1 V_{\text{Soret}}$. The difference between these, curve
20 66, shows the net effective movement of constituents along the path as a function of
45 diffusivity. The fast forward pumping efficiently moves low- and intermediate-
diffusivity constituents by virtue of the large number of cooler zones advancing per unit

time. The slower backward pumping culls the constituents that are too large to be of interest but were conveyed forward during the fast phase.

If the end of the pathway is blocked, the concentration of a constituent for which the net flux is positive increases at the blocked end until its back diffusion comes into equilibrium with its forward net pumping flux. FIG. 7 shows the calculated resulting concentration of dilute constituents in nitrogen as a function of constituent diffusivity. Constituents with values of diffusivity greater than that of RDX are not concentrated to any significant degree while those with smaller values are reverse-pumped to the rear of the pathway. By changing ΔT or V_{move} , other preselected constituents could be concentrated.

FIG. 8 shows, in cross-section, an apparatus 78 for pumping a chemical constituent from a fluid flowing in the direction indicated by arrows 79, as prescribed by the invention. A disk 80 opposes a parallel annulus 81 to form a radial pathway 82 therebetween, including a first end at the circumferential edges 102 and second end near the centers 100 of the disk 80 and annulus 81. The pathway 82 includes a passage 84 and an inlet area 103. The disk 80 and annulus 81 each comprise a substrate 85 and a thermally insulating layer 87, facing the pathway 82, over which is patterned a resistive material 90 forming distinct rings on the disk 80 and annulus 81, concentric around the center of the annulus 81. A temperature regulation system 93, such as is well known to those of skill in the art, is coupled to the resistive material 90 for controlling the respective temperature of each ring so as to generate a moving thermal profile. (Optionally only one of the disk 80 and the annulus 81 bears the resistive material 90.) A circular channel 95 through the center of the annulus 81 optionally

5 communicates with a sensing device 99 for analyzing the fluid composition delivered to
the center 100 of the annulus by the pumping apparatus 78. The apparatus 78 may
10 include a barrier 101 covering the channel 95 so as to allow a target constituent to
accumulate near the channel 95 and operated so as to periodically open and admit
15 components in the channel 95 into the sensing device 99. Other separated member
configurations, such as those including rectangular plates or members of other shapes,
with other pathway orientations, for example from one edge of a member to its opposite
20 edge, are also compatible with the invention.

An annulus 81 having a diameter of 2 cm with a channel diameter of 1 mm can
10 accommodate 950 concentric resistively heated rings each measuring 10 μm along the
25 radius. (Such micrometer-sized heating elements are known to those skilled in the art.
See, for example, J. S. Suehle *et al.*, in *IEEE Electron Device Letters* 14, 188-120
30 [1993] and R. E. Cavicchi *et al.*, *ibid* 16, 286-288 [1995]). Using six rings to create
each tooth 26 of the thermal profile shown in FIG. 4 would be appropriate for a spacing
15 s of about 20 μm between the disk 80 and the annulus 81; the length of the sawtooth 24
35 is preferably much larger than the spacing s in order to minimize smearing of the
thermal gradients in the direction perpendicular to the surface of the resistive material
40 90. Assuming that air passes over the edges 102 of the apparatus 78 at 600 cm s^{-1} , this
configuration would be able to concentrate a selected constituent by a factor as large as
20 10^5 , as shown in FIG. 7, in several tens of seconds. The concentrating power of the
45 apparatus 78 grows exponentially with the number of teeth 24 used along the passage
84. The small thermal time constants, less than 0.1 millisecond, of the heating elements
50 enable quick accumulation of a threshold concentration at the second end of the

5 pathway, near the centers 100 of the disk 80 and annulus 81. Larger resistive elements,
such as those measuring up to 20 μm , 50 μm , or 100 μm along the pathway are also
10 compatible with the apparatus of the invention.

In an alternate embodiment, the resistive material 90 is arranged on the disk 80
15 and/or the annulus 81 in continuous spiral or serpentine elements. Such a configuration
of two spiral elements 120 and 121 is shown in FIG. 9. The use of two or several
interspersed serpentine elements simplifies the operation of the temperature regulation
20 system 93 by reducing, compared to a concentric ring configuration, the number of
elements that must be individually addressed in forming the moving thermal profile.

10 The features and movement of the thermal gradient in the passage 84 are
25 constructed by the temperature regulation system 93 to selectively deliver a target
constituent or set of constituents to the center 100 of the annulus 81. In operation, the
30 extreme temperatures of the moving thermal profile are chosen to be sufficiently high
so as to inhibit adherence of the atmospheric components on the interior surfaces of the
15 disk and the annulus but sufficiently low to prevent thermal decomposition of the target
35 constituent.

In order to minimize power consumption, it is desirable that the substrate
40 portion 85 of the disk 80 and annulus 81 have an adjustable thermal conductivity, for
example by comprising a cavity (not shown) facing the insulating layer 87 with a
20 variably conductive medium such as air filling the cavity. An alternative is a solid
45 substrate of a moderately conductive material such as silicon.

The temperature regulation system 93 of an embodiment incorporating a 100-
50 nm-thick thermally insulating layer 87 of silicon dioxide or silicon nitride patterned

5 with 50-nm-thick resistive elements 90 of polysilicon, tantalum or chromium would
supply approximately 25 W of heater power and extract power at the same rate. The
10 modeled operating power is linearly dependent on the time required for constituent
concentration. For example, if reaching the desired concentration in 0.1 second
15 requires 25 W, then only 2.5 W is needed to achieve the same concentration in 1 s. If a
lower ultimate concentration can be tolerated, fewer zones are needed along the
pathway, and the power requirement is decreased. For example, if the ultimate
20 concentration factor is only 10, then only 5 W is required. The actual power
requirements may also depends on other variables such as the algorithm used to switch
10 the power to the resistive heaters 90.

25 Typically, the ability to detect a target constituent within a particular time
interval depends more upon the ability of the sensing device 99 to collect a minimum
30 detectable absolute amount of the target constituent than its ability to concentrate the
constituent by several orders of magnitude. Thus is preferable to sample a large
15 volume of fluid in order to detect a constituent quickly. A large separation between the
35 disk 80 and annulus 81 would facilitate sampling of the fluid flowing in the direction of
arrow 79 across the edge 101 of the apparatus 78. However, smaller separations would
40 allow larger thermal gradients to be generated, supporting more selective pumping of
the target constituent.

20 A spacing s of about 20 μm between the interior surfaces of the disk 80 and the
45 annulus 81 allows the resistive elements to generate sufficient thermal gradients to
effectively separate constituents from the fluid mixture. Preferably, the spacing s
50 increases near the exterior edges 102 to form a relatively wide inlet area 103 to

5 facilitate sampling a large volume of air in order to detect a target constituent quickly.

A suitable inlet area 103 would have a depth along the diameter of about 1 mm and a

10 width w on the order of 100 μm , giving a two-centimeter device a sampling area of 6

mm^2 . As fluid flows across the edge 102, a boundary layer forms, out of which the

15 components of the fluid diffuse into the inlet area and are pumped wholesale by the

moving thermal profile into the narrower passage 84. In congruity with the larger

spacing w , broader teeth 24, on the order of ten or twenty times longer than those in the

20 passage 84, are used, so generating smaller temperature gradients for the same extreme

temperatures. Also, since the purpose of the time-varying profile in the inlet area 103 is

10 to deliver components of the fluid without discrimination, to improve sampling by the

25 passage 84, this thermal profile is moved only away from the edges 102 and only at a

relatively slow wave velocity, less than the Soret velocity.

30 When the apparatus 79 is operated to selectively preconcentrate a target

constituent for transport down the passage 84, it may be desirable to couple the end of

15 the pathway at the center 100 of the annulus 81 to a sensor device 99. In general, the

35 sensor device 99 detects and determines the concentration of the target constituent

delivered by the preconcentrator. Many types of sensor devices suitable for use in

40 conjunction with the preconcentrator of the invention are known to those skilled in the

art. The ion mobility spectrometer ("IMS"), is one such sensor device. In this case, a

20 constituent laser ionizer for photoionizing the components concentrated near the

45 channel 95 may be adjoined to the apparatus 79 through an aperture, not shown, in the

disk 80.

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The ability of the thermophoretic apparatus to increase the concentration of the target constituent as well as to eliminate other interfering impurities, substantially increases the sensitivity of the resultant system over the sensor device alone. Also, the ability of the thermophoretic concentrator apparatus 79 of the invention to differentiate between components of a fluid mixture on the basis of diffusivity adds a new dimension to the detection and characterization abilities of IMS-based systems because it eliminates confusion between components having overlapping spectra.

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The thermophoretic concentrator of the invention has the ability to actively pump constituents out of the pathway 82 as well as pumping them toward the detector, making it possible to clear the system of gaseous impurities in less time than that required to detect a target constituent. Particle contamination can be burned or blown out by quickly increasing the temperature of the concentrator to several hundred degrees.

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It will therefore be seen that the foregoing represents a highly advantageous approach to collecting and sorting target constituents from a mixture in a carrier medium, especially for enhancing the detector sensitivity and selectivity of detecting very dilute constituents. The terms and expressions employed herein are used as terms of description and not of limitation, and there is no intention, in the use of such terms and expressions, of excluding any equivalents of the features shown and described or portions thereof, but it is recognized that various modifications are possible within the scope of the invention claimed. For example, the moving thermal profiles need not be symmetrical or sawtoothed in form; or rather than a gas, the medium from which the target constituent is sorted may be a liquid, a gel, or a solid—for example silicon

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What is claimed is:

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dioxide through which alkali metals diffuse. In such embodiments, the pathway may be defined within the fixed boundaries of the condensed phase. Furthermore, the pathway may be defined by a tube rather than by opposite members; the moving thermal profile may generated by moving wires or other elements instead of integral resistive elements.

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Claims

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CLAIMS

1. A method of concentrating a target chemical constituent from a mixture of components, the method comprising the following steps:
- providing a pathway over which components are free to move, the pathway having first and second ends;
 - controlling temperature so as to create consecutive warmer and cooler zones, along the pathway;
 - supplying the mixture of components to the pathway; and
 - moving the zones together along the pathway
 - toward the second end at a forward wave velocity, and then
 - toward the first end at a backward wave velocity,
- thereby preferentially conveying the target chemical constituent to the second end.
2. The method of claim 1 wherein the step of controlling temperature creates a series comprising a plurality of alternating warmer and cooler zones along the pathway, the step of moving the zones displacing the series along the pathway.
3. The method of claim 1 wherein the target chemical constituent has a Soret velocity and collects in a cooler region preferentially to in a warmer region.
4. The method of claim 3 wherein the forward wave velocity is greater than the Soret velocity and the backward wave velocity is less than the Soret velocity.

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1 5. The method of claim 1 wherein moving the zones toward the second end transports
2 the target constituent and moving the zones toward the first end transports at least one
3 component larger than the target constituent preferentially, at a greater rate than the
4 target constituent.

1 6. The method of claim 1 wherein the forward wave velocity is unequal to the
2 backward wave velocity.

1 7. The method of claim 1 wherein the step of controlling temperature creates a forward
2 thermal profile for moving toward the first end and a backward thermal profile for
3 moving toward the first end, the forward and backward thermal profiles being distinct.

1 8. The method of claim 1 wherein the target chemical constituent has an initial
2 concentration in the mixture of components, preferential conveyance of the target
3 constituent collecting at the second end an ultimate concentration of the target chemical
4 constituent equal to at least ten times the initial concentration.

1 9. The method of claim 1 wherein the target chemical constituent has an initial
2 concentration in the mixture of components, preferential conveyance of the target
3 constituent collecting at the second end an ultimate concentration of the target chemical
4 constituent equal to at least one hundred times the initial concentration.

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- 1 10. The method of claim 1 wherein the target chemical constituent has an initial
2 concentration in the mixture of components, preferential conveyance of the target
10 3 constituent collecting at the second end an ultimate concentration of the target chemical
4 constituent equal to at least one thousand times the initial concentration.

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- 1 11. The method of claim 1 wherein the target chemical constituent has an initial
2 concentration in the mixture of components, preferential conveyance of the target
20 3 constituent collecting at the second end an ultimate concentration of the target chemical
4 constituent equal to at least ten thousand times the initial concentration.

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- 1 12. The method of claim 1 wherein the target chemical constituent has an initial
2 concentration in the mixture of components, preferential conveyance of the target
30 3 constituent collecting at the second end an ultimate concentration of the target chemical
4 constituent equal to at least one hundred thousand times the initial concentration.

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- 1 13. The method of claim 1 further comprising repeating step d at least once.

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- 1 14. The method of claim 1 wherein the mixture is a gas.

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- 1 15. The method of claim 1 wherein the target constituent is an explosive or a
2 decomposition product thereof.

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- 1 16. The method of claim 1 wherein the target constituent is a drug or a decomposition
2 product thereof.

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- 1 17. The method of claim 1 wherein the mixture is a liquid.

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- 1 18. The method of claim 1 wherein the mixture is a gel.

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- 1 19. The method of claim 1 wherein the mixture is a solid.

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- 1 20. The method of claim 1 wherein the target constituent is an ion.

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- 1 21. The method of claim 1 further comprising the step of moving a temperature
2 gradient toward the first end, thereby clearing the pathway of extraneous components.

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- 1 22. The method of claim 1 further comprising sensing the target chemical constituent
2 preferentially conveyed to the second end.

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- 1 23. The method of claim 18 wherein an ion-mobility spectrometer senses the target
2 chemical constituent.

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- 1 24. The method of claim 4 wherein the forward wave velocity is several times the
2 Soret velocity.

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1 25. The method of claim 4 wherein the backward wave velocity is less than half the
2 Soret velocity.

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1 26. The method of claim 1 wherein moving the zones together along the pathway sorts
2 components of the mixture on the basis of diffusivity.

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1 27. A method of pumping a target chemical constituent along a pathway from a first
2 end toward a second end, the method comprising the steps of:
3 a. controlling temperature so as to create consecutive warmer zone cooler zones
4 along the path;
5 b. supplying the target chemical constituent to the pathway; and
6 c. displacing the zones together along the pathway toward the second end at a
7 wave velocity, target chemical constituent moving with the zones, thereby being
8 conveyed to the second end.

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1 28. An apparatus for concentrating a target chemical constituent from a mixture of
2 components, the apparatus comprising:
3 a. a pathway over which components are free to move, the pathway having first
4 and second ends;
5 b. a temperature control system configured to control temperature so as to
6 create consecutive warmer and cooler zones, along the pathway, and to move the zones
7 together along the pathway
8 i. toward the second end at a forward wave velocity, and then

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9 ii. toward the first end at a backward wave velocity,
10 thereby preferentially conveying the target chemical constituent to the second end.

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1 29. The apparatus of claim 28 wherein the temperature control system is configured to
2 create a series comprising a plurality of alternating warmer and cooler zones along the
15 3 pathway and to displace the series along the pathway.

20 1 30. The apparatus of claim 28 wherein the temperature control system comprises a
2 series of resistive heating elements positioned along the pathway, the elements being
25 3 addressed so as to move the zones.

1 31. The apparatus of claim 28 wherein the pathway is defined by two members, each
30 2 member having an interior surface facing the pathway, in opposition.

1 32. The apparatus of claim 31 wherein the temperature control system comprises
35 2 resistive heating elements lithographically defined on the interior surface of at least one
3 of the two members.

40 1 33. The apparatus of claim 32 wherein the resistive heating elements each have a
2 dimension less than 100 μm along the pathway.

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1 34. The apparatus of claim 32 wherein the resistive heating elements each have a
50 2 dimension less than 50 μm along the pathway.

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1 35. The apparatus of claim 32 wherein the resistive heating elements each have a
2 dimension less than 20 μm along the pathway.

1 36. The apparatus of claim 28 wherein the pathway includes a relatively narrow
2 passage and a relatively wide inlet area at the first end.

1 37. The apparatus of claim 36 wherein the temperature control system is configured to
2 create a passage thermal profile in the passage and an inlet thermal profile in the inlet
3 area, the passage thermal profile being distinct from the inlet thermal profile.

1 38. The apparatus of claim 36 wherein the temperature control system is configured to
2 move a thermal profile, comprising consecutive warmer and cooler zones, along the
3 pathway in the inlet area so as to deliver mixture of components to the passage.

1 39. The apparatus of claim 28 wherein the target constituent is an explosive or a
2 decomposition product thereof.

1 40. The apparatus of claim 28 wherein the target constituent is a drug or a
2 decomposition product thereof.

1 41. The apparatus of claim 28 wherein the target constituent is a drug or a
2 decomposition product thereof.

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1 42. The apparatus of claim 28 further comprising a sensing device for receiving sample
2 at the second end and detecting target constituent.

1 43. The apparatus of claim 42 wherein the sensing device comprises an ion-mobility
2 spectrometer.

1 44. The apparatus of claim 31 wherein the members are circular, the pathway being
2 oriented along the radii.

1 45. The apparatus of claim 32 wherein the resistive heating elements form concentric
2 rings.

1 46. The apparatus of claim 31 wherein the temperature control system comprises a
2 plurality of interspersed serpentine resistive heating elements.

1 47. An apparatus for concentrating a target chemical constituent from a mixture of
2 components, the target constituent having a diffusivity and a Soret velocity and
3 collecting in a cooler region preferentially to in a warmer region, the apparatus
4 comprising:

5 a. two circular members, each having a circumference and a center, in
6 opposition having interior surfaces defining therebetween a pathway along radii over

- 5
- 7 which components are free to move, the pathway having a first end at the
- 8 circumferences and a second end at the centers;
- 10
- 9 b. resistive material patterned on the interior surface at least one of the two
- 10 members, forming thereon concentric rings having a dimension of less than 50 μm
- 11 along the radius; and
- 12
- 13 c. a temperature regulation system configured to provide current to the resistive
- 13 material so as to create along the pathway consecutive warmer and cooler zones and to
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- 14 move the zones together along the pathway repeatedly
- 15
- 16 i. toward the second end at a forward wave velocity greater than the
- 25
- 16 Soret velocity, and then
- 17
- 18 ii. toward the first end at a backward wave velocity less than the Soret
- 18 velocity, transporting at least one component having a smaller diffusivity than that of
- 30
- 19 the target constituent preferentially, at a greater rate than the target constituent,
- 20 thereby preferentially conveying target chemical constituent to the second end.
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- 1 48. An apparatus for concentrating a target chemical constituent from a mixture of
- 2 components, the target constituent having a diffusivity and a Soret velocity and
- 3 collecting in a cooler region preferentially to in a warmer region, the apparatus
- 40
- 4 comprising:
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- 6 a. two circular members, each having a circumference and a center, in
- 45
- 6 opposition having interior surfaces defining therebetween a pathway along radii over
- 7 which components are free to move, the pathway having a first end at the
- 8 circumferences and a second end at the centers;
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- 9 b. resistive material patterned on the interior surface at least one of the two
- 10 members, forming thereon interspersed serpentine heating elements each having a
- 11 dimension of less than 50 μm along the radius; and
- 12 c. a temperature regulation system configured to provide current to the heating
- 13 elements so as to create along the pathway consecutive warmer and cooler zones and to
- 14 move the zones together along the pathway repeatedly
- 15 i. toward the second end at a forward wave velocity greater than the
- 16 Soret velocity, and then
- 17 ii. toward the first end at a backward wave velocity less than the Soret
- 18 velocity, transporting at least one component having a smaller diffusivity than that of
- 19 the target constituent preferentially, at a greater rate than the target constituent,
- 20 thereby preferentially conveying target chemical constituent to the second end.

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- 1 49. An apparatus for pumping a target chemical constituent along a course, the
- 2 apparatus comprising:
- 35 a. a pathway having first and second ends; and
- 3 b. a temperature control system configured to control temperature so as to create
- 40 consecutive warmer and cooler zones along the pathway and to displace the zones
- 4 together along the pathway toward the second end, target chemical constituent moving
- 5 with the zones, thereby being conveyed to the second end.
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1 50. The apparatus of claim 49 wherein displacing the zones together along the pathway
2 transports the target chemical constituent preferentially compared to at least one other
3 constituent on the basis of diffusivity.

1 51. The method of claim 27 wherein displacing the zones together along the pathway
2 transports the target chemical constituent preferentially compared to at least one other
3 constituent on the basis of diffusivity.

1 52. The apparatus of claim 28 wherein displacing the zones together along the pathway
2 sorts components of the mixture on the basis of diffusivity.

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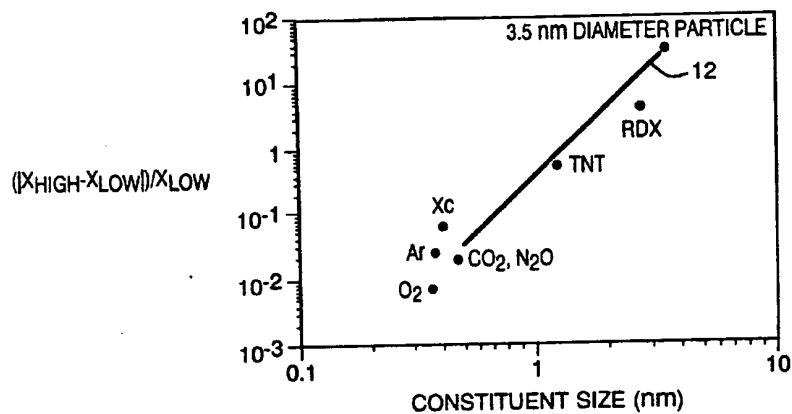


FIG. 1

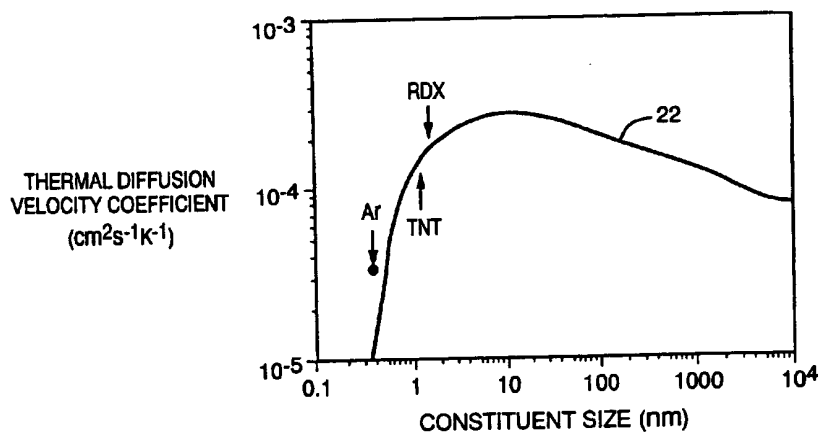


FIG. 2

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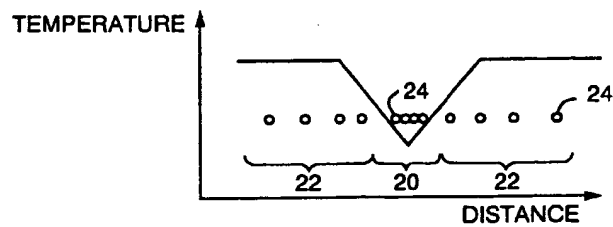


FIG. 3A

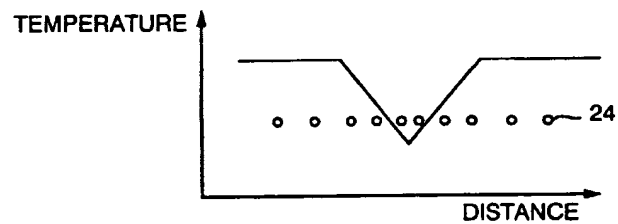


FIG. 3B

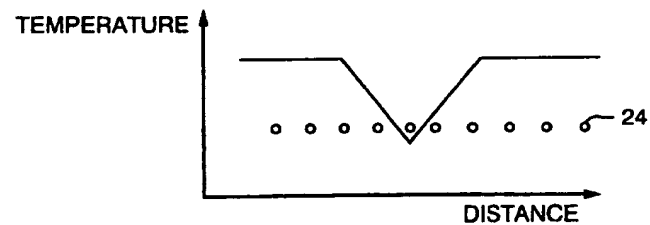


FIG. 3C

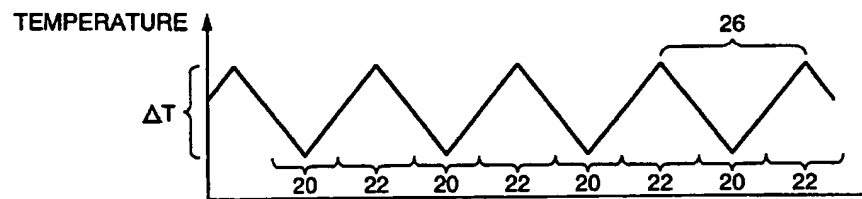


FIG. 4

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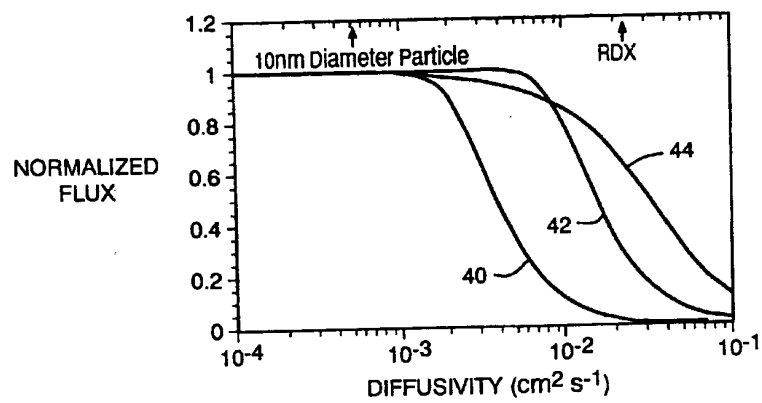


FIG. 5

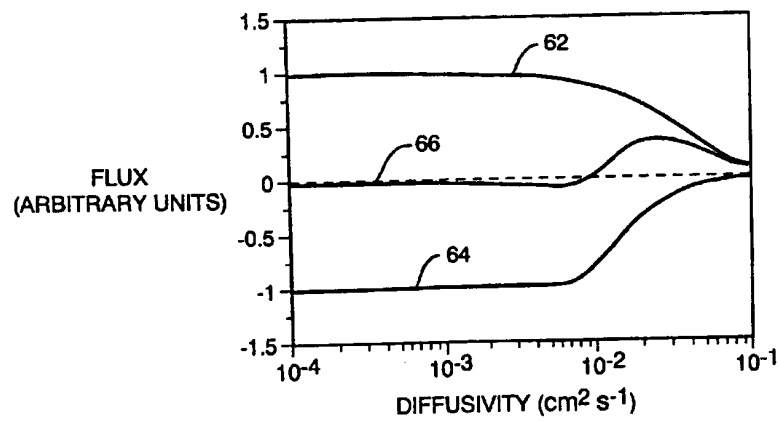


FIG. 6

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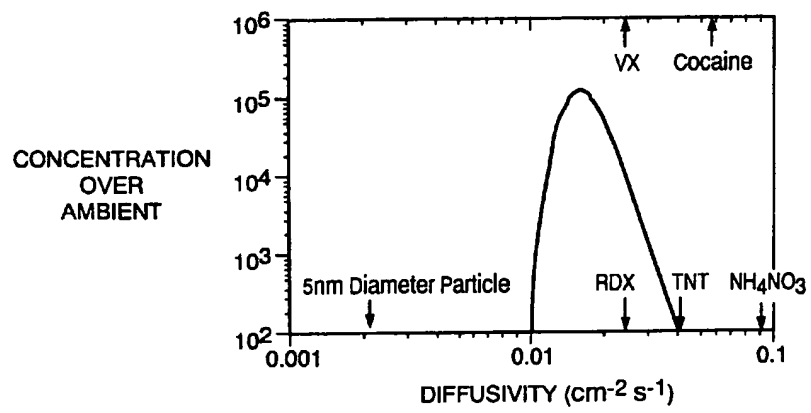


FIG. 7

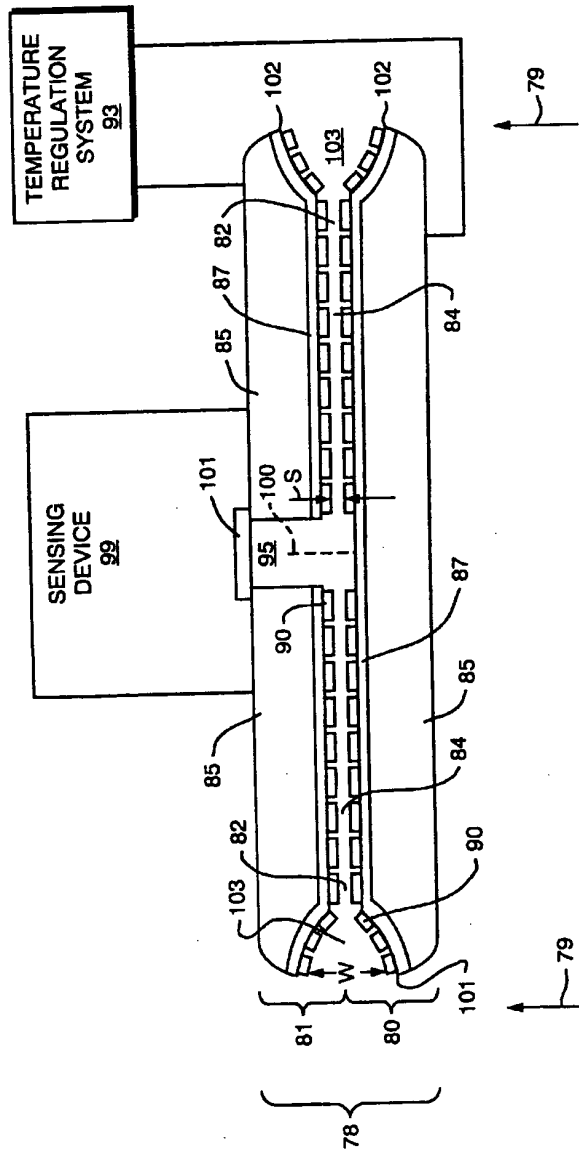


FIG. 8

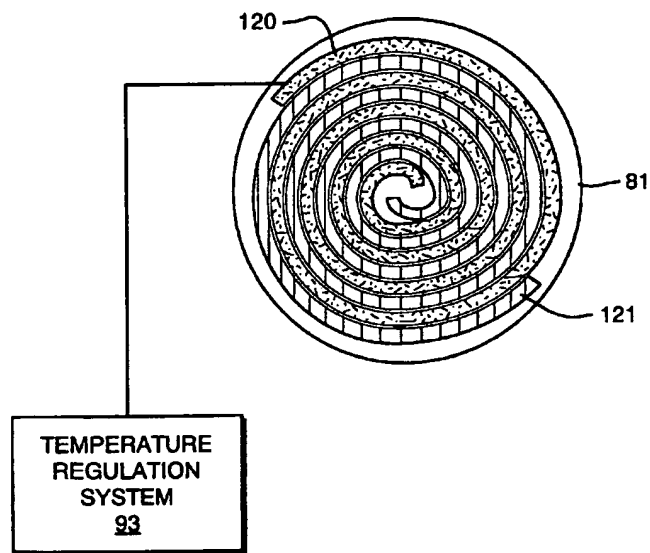


FIG. 9

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